

# Controlling Particle Trajectory in Free-Fall Electrostatic Separators

Laur Calin, Adrian Mihalcioiu, *Member, IEEE*, Subhankar Das, *Student Member, IEEE*, Vasile Neamtu, Ciprian Dragan, Lucian Dascalescu, *Senior Member, IEEE*, and Alexandru Iuga, *Senior Member, IEEE*

**Abstract**—The purity and recovery of concentrates obtained in industrial free-fall electrostatic separators can be increased by preventing the impacts between the particles and the electrodes. The aim of this paper is to analyze the possibility to control particle trajectories in such separators by modifying the conditions of particle admission in the interelectrode space. The parametric equations of a charged particle trajectory in the electric field between the electrodes of a free-fall separator served for writing a numerical modeling program in MATLAB. The ten control factors of the free-fall electrostatic separation process were employed as input variables of this program: particle charge and dimension, trajectory start point coordinates, feed input angle and initial velocity, electrode length and inclination, interelectrode spacing, and applied high voltage. A custom-designed laboratory free-fall electrostatic separator (length of the electrodes: 1000 mm; standard interelectrode spacing: 300 mm; and nominal high voltage: 90 kV), provided with a fluidized-bed tribocharger, was employed for validating the conclusions of the numerical mod-

eling. The geometrical data of this separator were taken into account for computing the initial velocity  $v_0$  of the particles entering the electric field zone. Another important parameter of the numerical model, which is the granule charge  $q$ , was attributed the value measured at the exit of the fluidized-bed tribocharger. The numerical simulations were performed for the two values of the feed input angle:  $\alpha = 4^\circ$  and  $\alpha = 8^\circ$ , considering polyethylene terephthalate (PET) and polyvinyl chloride (PVC) particles of different sizes. A good agreement was found between the theoretical predictions and the results of the experiments carried out with two binary mixtures: 50% PET/50% PVC and 10% PET/90% PVC. Both the numerical modeling and the experimental study demonstrated that the feed input angle  $\alpha$  influences the outcome of the electrostatic separation to a great extent.

**Index Terms**—Electrostatic processes, numerical simulation, particle trajectory, triboelectrostatic separator.

## I. INTRODUCTION

**A**N INCREASING number of applications, most of them in mineral processing [1]–[3] and recycling industries [4], [5], make use of free-fall electrostatic separators to take advantage of their relatively larger throughput capacity as compared with other types of installations (roll-type or plate-type electrostatic separators). The tribocharging device and the electrode system are essential elements characterizing the triboelectrostatic free-fall separator. Several technical solutions have been patented [6], [7] or described in the literature [8]–[11].

Industrial practice reveals the importance of the input feeder in obtaining high purity and recovery concentrates [12]. This can be easily explained by the fact that the trajectory of a charged particle in a free-fall electrostatic separator is influenced by the position in which the particle is introduced in electrostatic field and the initial particle velocity [13].

A delicate problem of the input feeder is the adjustment of the input angle  $\alpha$  (Fig. 1). When  $\alpha = 0$ , the light particles with the same mass but different positive charges describe distinct trajectories [Fig. 1(a)]. The normal trajectory of a positively charged particle ends in the compartment of the collector situated under the negative electrode.

The higher positively charged particles hit the negative electrode and are deviated as impurities in the collecting compartment located under the positive electrode or are retained by the image force on the negative electrode surface. If the angle  $\alpha$  is appropriately chosen [Fig. 1(b)], the collisions with the electrode can be avoided.

This paper presents the numerical simulation and the experimental study of charged-particle trajectories in a free-fall electrostatic separator for different feed input angles.

Paper MSDAD-07-48, presented at the 2006 ESA/IEEE/IEJ/SFE Joint Conference on Electrostatics, Berkeley, CA, June 20–23, and approved for publication in the IEEE TRANSACTIONS ON INDUSTRY APPLICATIONS by the Electrostatic Processes Committee of the IEEE Industry Applications Society. Manuscript submitted for review June 30, 2006 and released for publication October 30, 2007. Published July 23, 2008 (projected). The work of L. Calin was supported in part by the Technical University of Cluj-Napoca and in part by the University of Poitiers.

L. Calin is with the High-Intensity Electric Fields Laboratory, Technical University of Cluj-Napoca, 40020 Cluj-Napoca, Romania, and also with the Electronics and Electrostatics Research Unit, Laboratory of Automation and Industrial Informatics, University of Poitiers, University Institute of Technology, 16021 Angoulême, France (e-mail: laurflorintcalin@yahoo.com).

A. Mihalcioiu was with the Electronics and Electrostatics Research Unit, Laboratory of Automation and Industrial Informatics, University of Poitiers, University Institute of Technology, 16021 Angoulême, France, and was also with the High-Intensity Electric Fields Laboratory, Technical University of Cluj-Napoca, 40020 Cluj-Napoca, Romania. He is now with the Department of Ecological Engineering, Toyohashi University of Technology, Toyohashi 441-8580, Japan (e-mail: madrian@iutang.univ-poitiers.fr).

S. Das was with the Electronics and Electrostatics Research Unit, Laboratory of Automation and Industrial Informatics, University of Poitiers, University Institute of Technology, 16021 Angoulême, France. He is now with the General Electric Technology Center, Bangalore, India (e-mail: Subhankar.Das@ge.com).

V. Neamtu and A. Iuga are with the High-Intensity Electric Fields Laboratory, Technical University of Cluj-Napoca, 40020 Cluj-Napoca, Romania (e-mail: Alexandru.Iuga@et.utcluj.ro).

C. Dragan was with the Electronics and Electrostatics Research Unit, Laboratory of Automation and Industrial Informatics, University of Poitiers, University Institute of Technology, 16021 Angoulême, France. He is now with the Electrostatics of Dispersed Media Research Unit, Laboratory of Aerodynamic Studies, University of Poitiers, University Institute of Technology, 16021 Angoulême, France (e-mail: cipri.dragan@gmail.com).

L. Dascalescu was with the Laboratory of Automation and Industrial Informatics, University of Poitiers, University Institute of Technology, 16021 Angoulême, France. He is now with the Electrostatics of Dispersed Media Research Unit, Laboratory of Aerodynamic Studies, University of Poitiers, University Institute of Technology, 16021 Angoulême, France (e-mail: lidascalescu@iutang.univ-poitiers.fr).

Digital Object Identifier 10.1109/TIA.2008.926690

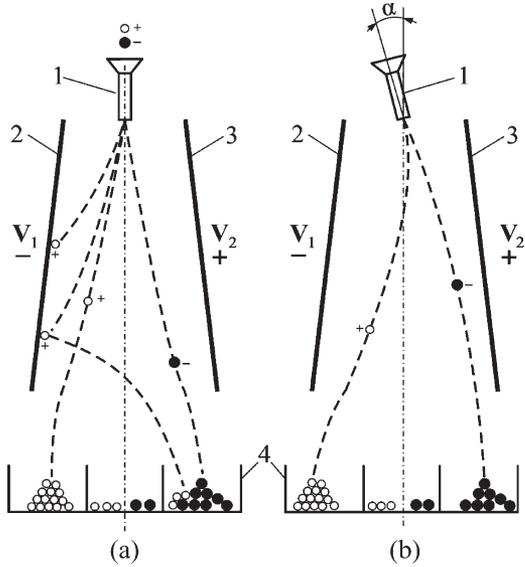


Fig. 1. Charged-granule trajectories in the electrostatic field of free-fall separator for (a) the vertical in-feed and (b) the inclined in-feed. 1) Adjustable angle input feeder. 2) and 3) Plate electrodes. 4) Collector.  $\alpha$ ) Feed input angle.

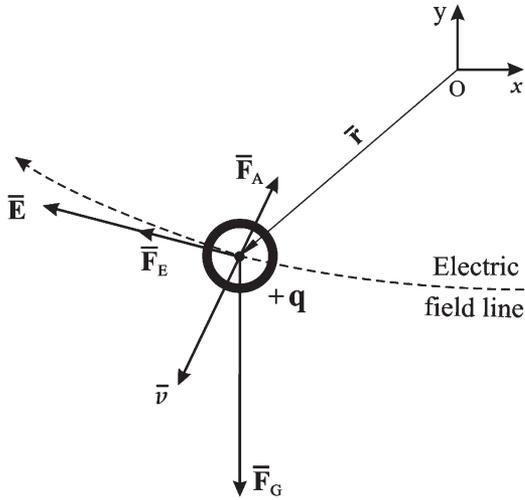


Fig. 2. Forces acting on a charged particle in a free-fall electrostatic separator.

## II. MATHEMATICAL MODEL OF PARTICLE TRAJECTORIES

The motion of a charged particle in the electrostatic field  $\mathbf{E}$  of the free-fall separator (Fig. 2) takes place under the action of the gravitational force  $\mathbf{F}_G$ , electrical field force  $\mathbf{F}_E$ , and air frictional force (drag force)  $\mathbf{F}_A$ , according to the vectorial equation

$$m \frac{d^2 \mathbf{r}}{dt^2} = \overline{\mathbf{F}}_G + \overline{\mathbf{F}}_E + \overline{\mathbf{F}}_A \quad (1)$$

where  $m$  is the particle mass, and  $\mathbf{r}$  is the position vector of particle mass center.

The magnitudes of the forces in (1) are given by the following:

$$F_G = mg \quad (2)$$

$$F_E = qE \quad (3)$$

$$F_A = \frac{1}{2} C_D \rho_A S v^2 \quad (4)$$

where  $g$  is the gravity acceleration,  $q$  is the particle charge,  $E$  is the electric field strength,  $C_D$  is the drag coefficient,  $\rho_A$  is the air density,  $S$  is the particle projected surface on motion direction, and  $v$  is the particle velocity.

The electrostatic field of free-fall separator has plan-parallel symmetry. Particle trajectory, described by the position vector  $\mathbf{r}(x, y)$ , represents a plane curve which may be approximated by linear segments. On each trajectory segment, corresponding to a time increment  $\Delta t$ , the motion is considered rectilinear and uniformly accelerated (acceleration is constant), and the velocity increases with a quantity  $\mathbf{a} \cdot \Delta t$ .

Thus, for the segment  $[i, i+1]$ , where the initial vectorial quantities  $\mathbf{r}_i(x_i, y_i)$ ,  $\mathbf{v}_i(v_{ix}, v_{iy})$ , and  $\mathbf{a}_i(a_{ix}, a_{iy})$  are known, the position vector of the point  $(i+1)$  is given by the vectorial equation

$$\overline{\mathbf{r}}_{(i+1)} = \overline{\mathbf{r}}_i + \overline{\mathbf{v}}_i \Delta t + \frac{1}{2} \overline{\mathbf{a}}_i \Delta t^2 \quad (5)$$

To determine the next point of trajectory  $\mathbf{r}_{(i+2)}$ , it is necessary to calculate the velocity  $\mathbf{v}_{(i+1)}$  and acceleration  $\mathbf{a}_{(i+1)}$  in the point  $(i+1)$

$$\overline{\mathbf{v}}_{(i+1)} = \overline{\mathbf{v}}_i + \overline{\mathbf{a}}_i \Delta t \quad (6)$$

$$\overline{\mathbf{a}}_{i+1} = \frac{1}{m} [\overline{\mathbf{F}}_G + \overline{\mathbf{F}}_{E(i+1)} + \overline{\mathbf{F}}_{A(i+1)}] \quad (7)$$

The trajectory parametric equations in Cartesian form, corresponding to the vectorial equations (5)–(7), are as follows:

$$\begin{cases} x_{(i+1)} = x_i + v_{ix} \Delta t + \frac{1}{2} a_{ix} \Delta t^2 \\ y_{(i+1)} = y_i + v_{iy} \Delta t + \frac{1}{2} a_{iy} \Delta t^2 \end{cases} \quad (8)$$

$$\begin{cases} v_{(i+1)x} = v_{ix} + a_{ix} \Delta t \\ v_{(i+1)y} = v_{iy} + a_{iy} \Delta t \end{cases} \quad (10)$$

$$\begin{cases} a_{(i+1)x} = \frac{1}{m} [-qE_{(i+1)x} + F_{A(i+1)x}] \\ a_{(i+1)y} = \frac{1}{m} [-mg + qE_{(i+1)y} + F_{A(i+1)y}] \end{cases} \quad (12)$$

$$\begin{cases} x_{(i+1)} = x_i + v_{ix} \Delta t + \frac{1}{2} a_{ix} \Delta t^2 \\ y_{(i+1)} = y_i + v_{iy} \Delta t + \frac{1}{2} a_{iy} \Delta t^2 \end{cases} \quad (9)$$

where

$$\begin{cases} F_{A(i+1)x} = \frac{1}{2} C_D \rho_A v_{(i+1)x}^2 \text{sign} [v_{(i+1)x}] \\ F_{A(i+1)y} = \frac{1}{2} C_D \rho_A v_{(i+1)y}^2 \text{sign} [v_{(i+1)y}] \end{cases} \quad (14)$$

$$\begin{cases} F_{A(i+1)x} = \frac{1}{2} C_D \rho_A v_{(i+1)x}^2 \text{sign} [v_{(i+1)x}] \\ F_{A(i+1)y} = \frac{1}{2} C_D \rho_A v_{(i+1)y}^2 \text{sign} [v_{(i+1)y}] \end{cases} \quad (15)$$

In the start point of the trajectory ( $i=0$ ), the initial quantities are as follows:

$$\begin{cases} \overline{\mathbf{r}}_0(x_0, y_0 = 0) \\ \overline{\mathbf{v}}_0(v_{0x} = v_0 \sin \alpha, v_{0y} = -v_0 \cos \alpha) \\ \overline{\mathbf{a}}_0(a_{0x} = 0, a_{0y} = -g). \end{cases} \quad (16)$$

Particle trajectory, as can be observed in (12), (13), and (16), depends on the electric field strength ( $E_x, E_y$ ), the particle charge  $q$ , the particle mass  $m$ , the input position  $(x_0, y_0)$ , the initial velocity  $v_0$ , and the input angle  $\alpha$ .

The parametric equations of trajectory (8) and (9) are differential equations of second order that can be integrated by an approximation method using MATLAB 7.0. The original program, written by authors, simulates the 2-D trajectory of a particle in free-fall separator.

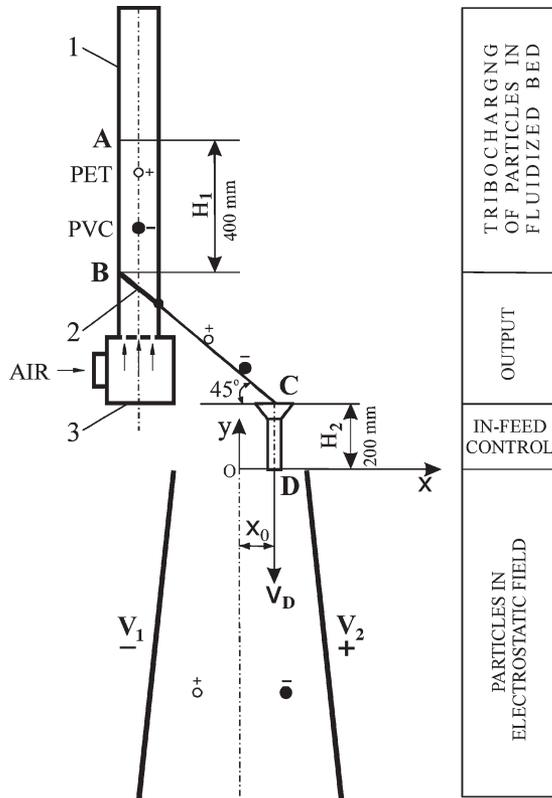


Fig. 3. Schematic representation of the free-fall triboelectrostatic separator.

The Cartesian components of electric field strength, in each point of trajectory, were determined by approximating the field lines by circular arcs. The time increment  $\Delta t$  was chosen 1 ms.

The input data for trajectory simulation are the following: the length of the plate electrodes, the vertical inclinations of the electrodes, the interelectrode gap, the initial point coordinates of trajectory, the particle initial velocity, the feed input angle, the particle charge, the particle diameter, the mass density of the particle, the potential difference between electrodes, the drag coefficient, and the air density.

Particle initial velocity  $v_0$  and particle charge  $q$  are application specific quantities, which are evaluated and measured further, as shown in the next section of this paper.

### III. MATERIALS AND METHOD

#### A. Granules Characterization

The materials used for trajectory study in free-fall separator (Table I) are millimeter-size virgin granules of polyethylene terephthalate (PET) and polyvinyl chloride (PVC). By using PET and PVC granules of different colors, it was easier to analyze the purity and the extraction of the concentrates in the electrostatic separation tests.

The average mass of the granules was experimentally determined by weighting 1000 particles.

#### B. Experimental Setup

The tribocharging process of the PET/PVC mixture was carried out in a fluidized-bed device [14]. Charging is mainly

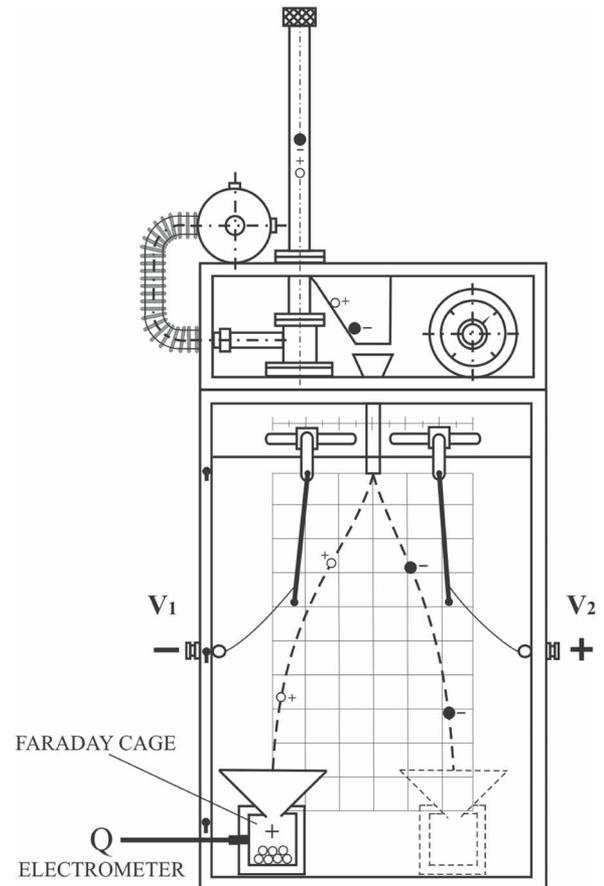


Fig. 4. Experimental setup for evaluating the electrical charge of the granules.

produced by multiple collisions between PET and PVC particles. However, the charge of the particles is amplified in contact with polypropylene (PP) walls of the tribocharging chamber, as PVC is located on the left side and PET on the right side of PP in triboelectric series [15] (Table I). By opening the output door of the fluidized-bed device, the charged particles leave the tribocharging chamber by free-fall motion, slide freely along an inclined plane at  $45^\circ$ , enter in the adjustable input feeder, and are introduced in the electrostatic field of the free-fall separator (Fig. 3).

In a first group of experiments, aimed at estimating the charge/mass ration, the standard 1000-mm plate electrodes, vertically inclined at  $5^\circ$  and spaced at 300 mm, were replaced by shorter ones (400 mm in length), so that a Faraday cage, connected to a digital electrometer, could be placed under the electrodes in the collecting zone (Fig. 4). Eight samples, consisting of 25 g of PET and 25 g of PVC, were prepared for these measurements. To determine the PET particle charge, the Faraday cage was located under the negative electrode. Each 50-g sample was tribocharged for 60 s in the fluidized-bed device, using the air generated by a turbo blower at  $38^\circ\text{C}$  and 20% relative humidity. Charged granular mixture was introduced in the electrostatic field of separator by means of the input feeder, adjusted to  $\alpha = 0$ . Under the action of the separation forces, the PET particles were deviated toward the negative electrode. In the Faraday cage, PET particles were collected only. The charge  $Q$  indicated by the electrometer was

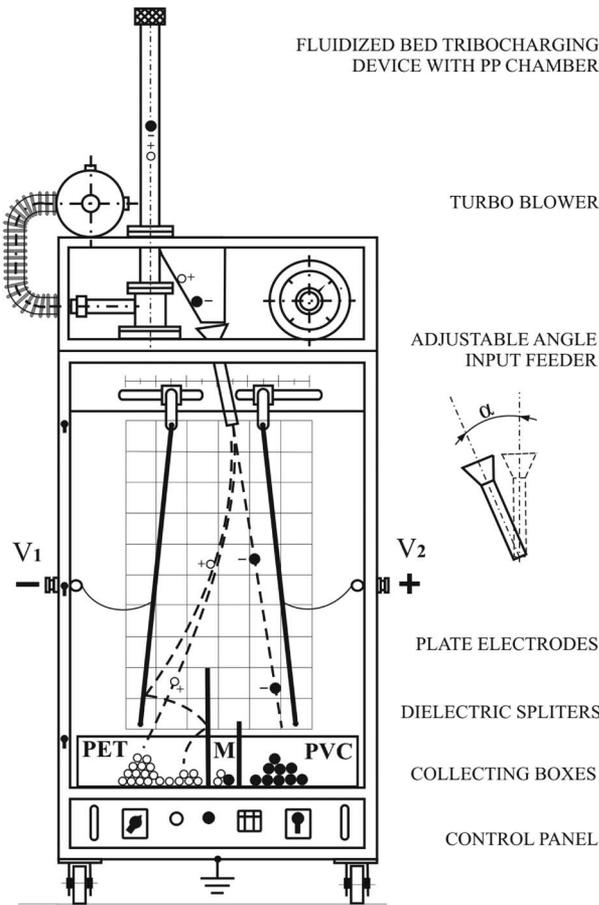


Fig. 5. Free-fall electrostatic separator equipped for the experiments of particle trajectory control by adjusting the input angle  $\alpha$ .

divided to the mass  $m$  measured by an electronic balance and to the number  $N$  of PET particles in a gram to determine the charge  $q$  of a PET particle

$$q = (Q/m)/N. \tag{17}$$

This procedure was repeated four times to find out the minimum, maximum, and average charges of PET particle.

To evaluate the PVC particle charge, the Faraday cage was located under the positive electrode. Another set of four experiments was performed using the same procedure consisting in tribocharging, electrostatic separation, and charge measurement.

The second set and third sets of experiments were done with the standard electrode configuration of the laboratory free-fall electrostatic separator (Fig. 5). Their aim was to evaluate the efficiency of the electrostatic separation at various values of the feed input angle ( $\alpha = 0^\circ, 4^\circ,$  and  $8^\circ$ ). A 400-mm-length dielectric splitter was located 30 mm on the left side of separator symmetry axis in order to prevent that the PET particles that hit the negative electrode are deviated in the middling (M) or the PVC concentrate. A second 200-mm splitter prevents the jumps of particles between M and PVC compartments. The other conditions were similar to those described for the first set of experiments. Samples containing 50% PET and 50% PVC were employed in the second set of experiments, whereas

TABLE I  
PHYSICAL CHARACTERISTICS OF PLASTIC GRANULES

Material	PET	PVC
Colour	White	Yellow
Size [mm]	2.5x2x2	Ø4.5x1.4
Mass [mg]	13.3	30.5
Mass density [kg/m <sup>3</sup> ]	1330	1370
Triboelectric series	- PVC ● PP ● PET +	
Equivalent diameter [mm]	2.86	4.06
Number of granules per gram	75	33

TABLE II  
CHARGE ON PET AND PVC GRANULES ( $\alpha = 0^\circ$ ; 50% PET/50% PVC)

PET (Plus)	Q/m	16.32	19.82	16.08	18.26	Avr
	[nC/g]					
q	0.217	0.264	0.214	0.243	0.235	
[nC]		Max	Min			
PVC (Minus)	Q/m	15.03	16.18	16.22	16.09	Avr
	[nC/g]					
q	0.458	0.493	0.495	0.491	0.484	
[nC]	Min		Max			

the third one was done with 10% PET/90% PVC granular mixtures.

#### IV. EXPERIMENTAL RESULTS

##### A. Charge Measurements

The results of the tribocharging process of the 50% PET/50% PVC mixture are given in Table II.

##### B. Electrostatic Separation Experiments

Table III contains the results of the set of experiments carried out with the 50% PCV/50% PET samples. The purities and recoveries of both concentrates were better when  $\alpha$  increased due to the diminishing number of elastic collision of PET particles with the negative electrode and to the barrier effect of the 400-mm splitter. This set of experiments pointed out the displacement of trajectories toward the positive electrode when the angle  $\alpha$  increased, an effect that will be observed also in numerical simulation. The best results were obtained for  $\alpha = 8^\circ$ .

The results of the last group of experiments, shown in Table IV, revealed an increase of purity and recovery for both concentrates obtained from the 10% PET/90% PVC, when the input angle  $\alpha$  varies from  $0^\circ$  to  $8^\circ$ .

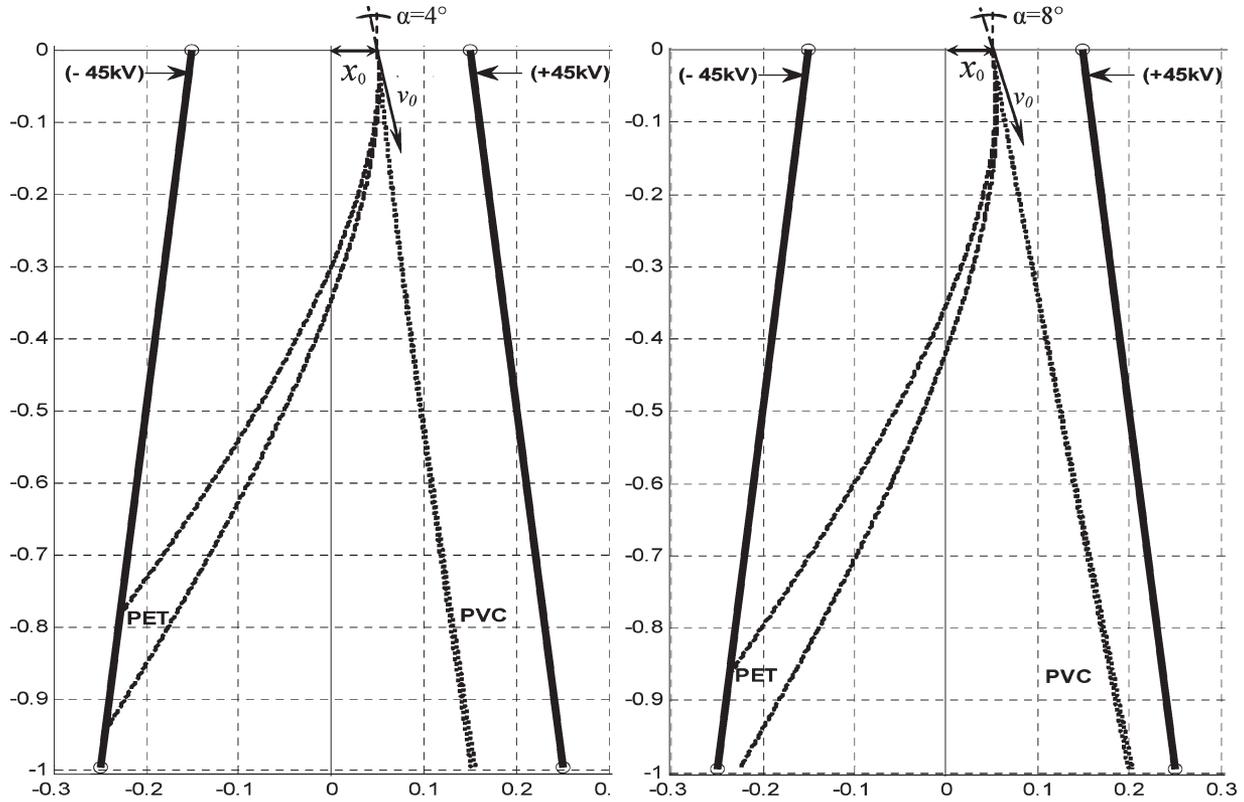


Fig. 6. MATLAB-plotted trajectories of PET and PVC particles for minimum and maximum charges and two input angles. The trajectories corresponding to the maximum charges are more deviated toward the electrodes due to stronger electrical forces.

TABLE III  
RESULTS OF THE ELECTROSTATIC SEPARATION EXPERIMENTS  
CARRIED OUT WITH THE 50% PET/50% PVC SAMPLES  
(AVERAGE OF FIVE EXPERIMENTAL RUNS EACH)

Products	$\alpha = 0^\circ$		$\alpha = 4^\circ$		$\alpha = 8^\circ$	
	PET	PVC	PET	PVC	PET	PVC
Purity	98.8	93.3	98.8	93.7	99.6	96.1
Recovery	61.8	69.4	69.3	74.3	70.0	81.6

TABLE IV  
RESULTS OF THE ELECTROSTATIC SEPARATION EXPERIMENTS  
CARRIED OUT WITH THE 10% PET/90% PVC SAMPLES  
(AVERAGE OF FIVE EXPERIMENTAL RUNS EACH)

Products	$\alpha = 0^\circ$		$\alpha = 4^\circ$		$\alpha = 8^\circ$	
	PET	PVC	PET	PVC	PET	PVC
Purity	98.8	93.3	98.8	93.7	99.6	96.1
Recovery	61.8	69.4	69.3	74.3	70.0	81.6

V. NUMERICAL SIMULATION OF PARTICLE TRAJECTORIES

The initial velocity  $\nu_0$  was calculated under certain assumptions (Fig. 3).

- 1) When the compressed air that supplies the fluidized-bed tribocharging device is turned off, the particles begin to fall freely in the tribocharging chamber from the average height  $H_1$  with an initial velocity  $\nu_A = 0$ .
- 2) During particle movement on the inclined plane at the output of the tribocharging chamber, the velocity remains constant, as the tangential component of gravitational force is balanced by frictional force.
- 3) Adjustable input feeder is vertically positioned ( $\alpha = 0$ ), and its output velocity is the initial velocity of the particles falling freely in the electric field of the separator ( $\nu_0 \approx \nu_D$ ).

The computation was performed by taking into account the conversion of the initial potential energy of the particle in point A into kinetic energy. Thus,

$$\nu_B = \sqrt{2gH_1} \tag{18}$$

$$\nu_C = \nu_B \cos^2 45^\circ = \frac{1}{2}\nu_B \tag{19}$$

$$\nu_0 \approx \nu_D = \sqrt{g(2H_2 + H_1/2)} = 2.4 \text{ m/s.} \tag{20}$$

The value given by (20) was introduced in the program that computed the particle trajectories for an electrode configuration similar to the one considered for the experiments presented in Section IV-B.

- 1) Electrode length is 1 m.
- 2) Interelectrode spacing is 0.3 m.
- 3) Vertical inclination of the electrodes is  $5^\circ$ .
- 4) Potentials of the electrodes are  $V_1 = -45 \text{ kV}$  and  $V_2 = +45 \text{ kV}$ .

The PET and PVC particles were approximated with equivalent spheres; the mass and equivalent diameter of which are given in Table I. The minimum and maximum charges of a type of particles were chosen as the extreme values in the series of four tests (Table II). The other input data were the drag coefficient ( $C_D = 0.4$ ), the air density ( $\rho_A = 1.22 \text{ kg/m}^3$ ), the coordinates of the starting point ( $x_0 = 0.05 \text{ m}$ ;  $y_0 = 0$ ), and the initial velocity ( $v_0 = 2.4 \text{ m/s}$ ).

The results of the numerical simulations can be examined in Fig. 6. The most affected by the electrostatic field were the trajectories of the PET particles carrying the maximum charge because of the higher ratio between the electrical and gravitational forces  $F_{E \text{ max}}/F_G$ . An increase of input angle from  $\alpha = 4^\circ$  to  $\alpha = 8^\circ$  rotates the assembly of the trajectories toward the positive electrode, so that the trajectory of the PET particle with minimum charge has no contact with the negative electrode.

## VI. CONCLUSION

The efficiency of free-fall triboelectrostatic separators depends not only on the charge acquired by the particles in the tribocharging device and the strength of the electrostatic field between the electrodes but also on the position and the configuration of the input feeder. The ideal separation of a binary mixture implies control of these three groups of factors for obtaining two distinct sets of particle trajectories.

An original simulating program of the particle trajectory in free-fall triboelectrostatic separator enabled the plot of particle trajectories by taking into consideration more than ten control variables. Numerical simulation and the experimental study of separation trajectories for two types of particles tribocharged in a fluidized-bed device pointed out the importance of field input angle  $\alpha$  to improve the separation efficiency.

Both the experimental data and the computed results prove that the adjustment of the feed input angle may contribute significantly to a successful separation of a binary mixture of granular materials characterized by different particle masses or/and mixture ratios.

## ACKNOWLEDGMENT

The authors would like to thank students D. Moldovan and R. Beluga for their kind help in the experiments and graphics.

## REFERENCES

- [1] *The T-STAT Free-Fall Electrostatic Separator*. [Online]. Available: <http://www.otokumputechnology.com>
- [2] A. Singular and G. Fricke, "Die electrostatistische Aufbereitung von Kalihydroxidsalzen (Electrostatic processing of raw potash salt)," *Chem. Ing. Tech.*, vol. 55, no. 1, pp. 39–45, Jan. 1983.
- [3] K. B. Tennal, M. K. Mazumder, D. Lindquist, J. Zhang, and F. Tendeku, "Triboelectric separation of granular materials," in *Conf. Rec. IEEE IAS Annu. Meeting*, Oct. 1997, vol. 3, pp. 1724–1729.
- [4] *The V-STAT Electrostatic Separator for Plastic*, Carpc Inc., Jacksonville, FL, Prod. Bull., 1997.
- [5] L. Dascalescu, "Electrostatic separation of plastic from industrial wastes. A review," *J. Electrostat. Jpn.*, vol. 25, pp. 282–288, 2001.
- [6] R. Kohnlechner and L. Dascalescu, "New applications for standard electrostatic separators," in *Conf. Rec. IEEE IAS Annu. Meeting*, Hong Kong, Oct. 2005, vol. 4, pp. 2569–2572.
- [7] I. I. Inculet, G. S. P. Castle, and J. D. Brown, "Electrostatic separation of mixed plastic waste," U.S. Patent 5 289 922, Mar. 1, 1994.
- [8] K. Haga, "Applications of the electrostatic separation technique," in *Handbook of Electrostatic Processes*, J. S. Chang, A. J. Kelly, and J. M. Crowley, Eds. New York: Marcel Dekker, 1995, pp. 365–386.
- [9] B. A. Kwetkus, "Particle triboelectrification and its use in the electrostatic separation process," *Part. Sci. Technol.*, vol. 16, no. 1, pp. 55–67, 1998.
- [10] I. I. Inculet, G. Castle, and J. D. Brown, "Electrostatic separation of plastics for recycling," *Part. Sci. Technol.*, vol. 16, no. 1, pp. 91–100, 1998.
- [11] Y. Higashiyama, Y. Ujiie, and K. Asano, "Triboelectrification of plastic particles on vibrating feeder laminated with a plastic film," *J. Electrostat.*, vol. 42, no. 1/2, pp. 63–68, Oct. 1997.
- [12] A. I. Anghelov and I. N. Nabiulin, "Elektrostaticheskie separatory svobodnogo padeniya," in *Free-Fall Electrostatic Separators*. Moscow, Russia: Nedra, 1970.
- [13] J. Wei and M. J. Realf, "Design and optimization of free-fall electrostatic separators for plastic recycling," *Amer. Inst. Chem. Eng. J.*, vol. 49, no. 12, pp. 3138–3149, 2003.
- [14] A. Iuga, L. Calin, V. Neamtu, A. Mihalcioiu, and L. Dascalescu, "Tribocharging of plastic granulates in a fluidized bed device," *J. Electrostat.*, vol. 63, no. 6–10, pp. 937–942, Jun. 2005.
- [15] L. Calin, L. Caliap, V. Neamtu, R. Morar, A. Iuga, A. Samuila, and L. Dascalescu, "Tribocharging of granular plastic mixtures in view of electrostatic separation," in *Conf. Rec. IEEE IAS Annu. Meeting*, Hong Kong, Oct. 2005, vol. 2, pp. 1435–1441.



**Laur Calin** received the M.S. and Advanced Studies degrees in electronics and telecommunications engineering from the Technical University of Cluj-Napoca, Cluj-Napoca, Romania, in 1997 and 1998, respectively. In 2008, he received the Ph.D. degree in electrical engineering with a thesis on the particle tribocharging phenomena in electrostatic separation processes. His thesis was jointly sponsored by the Technical University of Cluj-Napoca and the University of Poitiers, France.

His main interests are triboelectrostatic effects, corona charging of particulates, and optimization of electrostatic separation processes.



**Adrian Mihalcioiu** (S'04–M'06) received the M.S. degree in electrical engineering from the Technical University of Cluj-Napoca, Cluj-Napoca, Romania, in 2002, the Ph.D. degree from the University of Poitiers, Poitiers, France, in 2005, and the Dr. Eng. degree (*magna cum laude*) from the Technical University of Cluj-Napoca, in December 2005. His graduate research work was carried out at the Electronics and Electrostatics Research Unit, University Institute of Technology, Angoulême, France, within the framework of the ERASMUS Student Mobility

Programme, financed by the European Community. His Ph.D. research work was jointly sponsored by the University of Poitiers and the Technical University of Cluj-Napoca. His dissertation research involved the development of measurement techniques and virtual instrumentation for the study and control of electrostatic processes.

He was with the University of Osaka, Japan, as a Postdoctoral Fellow. He currently holds a Postdoctoral Position with the Department of Ecological Engineering, Toyohashi University of Technology, Toyohashi, Japan.



**Subhankar Das** (S'05) received the B.E. degree in electrical engineering (with first-class honors) from the Faculty of Electrical Engineering, College of Engineering and Management, Kolaghat, India, in 2002, the M.Sc. (Eng.) degree in electrical engineering from the Indian Institute of Science, Bangalore, India, in 2004, and the Ph.D. degree, benefiting from a scholarship jointly sponsored by the French Government and industry, from the University of Poitiers, Poitiers, France, in November 2007, with a dissertation focused on electrostatic separation.

From September 2005 to July 2006, he was associated with a major project in the R&D Department of Hamos GmbH, Penzberg, Germany. Since January 2008, he has been with the General Electric Technology Center, Bangalore. His current research interests include electrical discharge and electrostatics applications, field computation, fine-particle charging, and nonthermal plasma processes.



**Vasile Neamtu** received the M.S. degree in electrical engineering and the Dr. Eng. degree in electrical technologies from the Technical University of Cluj-Napoca, Cluj-Napoca, Romania, in 1975 and 2000, respectively.

After six years spent in industry, as a Research and Development Engineer, he moved to the Technical University of Cluj-Napoca, first as Teaching Assistant, then a Lecturer and an Associate Professor. Since 2007, he has been a Professor with the Electrical Engineering Department. He has coauthored more than 20 papers, most of them related to the design of the electrodes and the high-voltage supplies of electrostatic separators of granular mixtures, with applications in the field of mineral processing and recycling industry.



**Ciprian Dragan** received the M.S. degree in electrical engineering from the Technical University of Cluj-Napoca, Cluj-Napoca, Romania, in 2006 and the Master's degree in automatics and signal processing from the University of Poitiers, Poitiers, France, in June 2007, where he is currently working toward the Ph.D. degree in the Laboratory of Aerodynamic Studies with a scholarship from the Poitou-Charentes Regional Council. His graduate research work was carried out at the Electronics and Electrostatics Research Unit, University Institute of Technology,

Angoulême, France, within the framework of the ERASMUS Student Mobility Programme, which was financed by the European Community.

At the University of Poitiers, he took part in two research projects aimed at the study of tribocharging phenomena and the development of novel electrostatic separation technologies.



**Lucian Dascalescu** (M'93–SM'95) received the M.S. degree (Hons.) in electrical engineering from the Technical University of Cluj-Napoca, Cluj-Napoca, Romania, in 1978, the Dr. Eng. degree in electrotechnical materials from the Polytechnic Institute of Bucharest, Bucharest, Romania, in 1991, and the Dr. Sci. degree and the "Habilitation à Diriger de Recherches" diploma both in physics from the University "Joseph Fourier," Grenoble Cedex, France, in 1994 and 1996, respectively.

From 1978 to 1982, he was with the Combinatul de Utilaj Greu [CUG (Heavy Equipment Works)], Cluj-Napoca. In 1983, he joined the Technical University of Cluj-Napoca, where he was initially an Assistant Professor, and then, became an Associate Professor of electrical engineering. From October 1991 to June 1992, he was with the Laboratory of Electrostatics and Dielectric Materials (LEMD), Grenoble, France, as a Research Fellow. He was an Invited Research Associate and a Lecturer at Toyohashi University of Technology, Toyohashi, Japan, and also a Visiting Scientist at the University of Poitiers, Poitiers, France. From 1994 to 1997, he was with the University Institute of Technology, Grenoble, where he taught electromechanical conversion of energy. In September 1997, he was appointed as a Professor of Electrical Engineering and Automated Systems, and the Head of the Electronics and Electrostatics Research Unit at the University Institute of Technology, Angoulême, France. From 1999 to 2003, he was the Head of the Department of Management and Engineering of Manufacturing Systems. Currently, he is the Head of the Electrostatics of Dispersed Media Research Unit, which is part of the Electrohydrodynamic (EHD) Group, Laboratory of Aerodynamic Studies, University of Poitiers. He is the author of several textbooks in the field of electrical engineering and ionized gases. He holds 14 patents and has authored or coauthored more than 80 journal papers, and was invited to lecture on the electrostatics of granular materials at various universities and international conferences.

Prof. Dascalescu is a Senior Member of the IEEE Industry Applications Society (IAS) and the Chair of the Electrostatics Processes Committee. He is a member of the Electrostatics Society of America, the Electrostatics Society of Romania, the Société des Electriciens et Electroniciens (SEE), and the Club Electrotechnique, Electronique, Automatique (EEA), France.



**Alexandru Iuga** (M'93–SM'99) received the M.S. degree in electromechanical engineering from the Mining Institute of Petrosani, Petrosani, Romania, in 1966, the M.S. degree in physics from the University of Cluj-Napoca, Cluj-Napoca, Romania, in 1974, and the Doctor of Engineering degree in fundamentals of electrical engineering from the Polytechnical Institute of Iasi, Iasi, Romania, in 1984.

Since 1968, he has been with the Technical University of Cluj-Napoca, where he is currently Professor Emeritus with the Department of Electrical Engineering and Head of the High-Intensity Electric Fields Laboratory. He has visited several universities in Poland, France, Italy, the U.K. and the U.S. He was the Invited Speaker at the Electrostatic Processes Committee Meeting of the IEEE Industry Applications Society, New Orleans, LA, September 25, 2007. He is coauthor of several books, more than 70 technical papers, and is the holder of ten patents on electrical separation equipment and technology.

Dr. Iuga is a member of the Electrostatics Society of America and a cofounder of the Electrostatics Society of Romania.